Nanofiltration Followed By Electrical Discharge Plasma for Destruction of PFAS and Co-Contaminants in Groundwater: A Treatment Train Approach

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DMAX PLASMA

Technical Objectives



What's Needed?

Since PFAS plumes are generally dilute (often a few ppb), remediation of PFAS-impacted water best lends itself to a treatment train approach with integrated *PFAS concentration and destructive steps*

Our Objective

- Demonstrate and validate a field-scale integrated treatment approach:
 - 1 Nanofiltration to concentrate PFAS and co-contaminants
 - Electrical Discharge Plasma to treat concentrate
- 3 "Apple to Apples" Bench-scale comparison of Electrochemical Oxidation and Plasma



Technical Objectives





Today's Presentation...



- Overview: Nanofiltration and Enhanced Contact Plasma technologies
- 2 Source water characterization
- 3 Treatability testing results
- 4 Next steps



Coupling Concentration & Destruction





KEY There are numerous opportunities to combine concentration and destructive*POINT:* technologies for the treatment of PFAS-impacted waters

Nanofiltration: The Basics





- High-pressure separation process where solutes are retained by membranes and concentrated into a smaller volume of water (*retentate or concentrate*)
- Majority of feed water exits system as treated *permeate (or filtrate)*
- *% Recovery:* proportion of feed water recovered as permeate
- *% Rejection:* proportion of solute (PFAS) retained by the membranes



Closed-Circuit Desalination (CCD)

Newer membrane systems such as closed-circuit desalination (CCD) can achieve >20x concentration of PFAS-impacted waters



Semi-Batch Treatment Process

MINES

- During filtration, concentrate recirculated internally, concentrate valve closed
- Once a recovery (proportion of feed water recovered as permeate) setpoint is reached, concentrate valve opens
- With concentrate valve open, plug-flow flush displaces concentrate in system
- Concentrate valve closes, new cycle starts

GSI

ENVIRONMENTA

Enhanced Contact Plasma: The Basics



Plasma-based water treatment uses electricity to:

- convert water into a mixture of highly reactive species (i.e., plasma)
- rapidly and non-selectively degrade recalcitrant organic contaminants
- 2 Plasma Formation: High voltage is applied between suspended electrodes (above the water surface) and submerged grounded electrodes

Plasma Reactor Components

- High voltage electrodes for generation of plasma
- > Stainless steel strips as grounded electrodes
- Gas diffusers for bubble formation to drive PFAS to liquid surface



Source Water Characterization







- Samples collected from several extraction wells
- Most abundant PFAS: PFOS, 6:2 FTS, and PFHxS
- Elevated alkalinity, calcium, and iron

Bench-scale Treatability Testing





Nanofiltration: *Membrane Concentration Tests*





- > Tested two membranes: NF-90 (tight NF) and CR-100
- > System uses 0.14 m² of flat-sheet membrane in two cells
- Each sequence produced ~3.6 L of permeate, ~0.4 L of concentrate
- > SCADA logs flow rate, pressure, conductivity, temperature
- Performed approximately 30 sequences up to 90% recovery
- Collected permeate and concentrate samples



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Nanofiltration: **Operational Results**





KEY No decrease in permeability was observed for both membranes indicating that*POINT:* CCD treatment of pretreated groundwater did not result in membrane fouling.

Nanofiltration: *Performance Results*



Permeate

Treated

Nanofiltration

Retentate

2

Feed





Nanofiltration: *Performance Results*



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- Concentrations of most PFAS in the CR100 permeate were below respective detection limits (Rejection ≈ 1)
- Two exceptions: PFPeA and PFBA (Rejection = 0.96 and 0.88, respectively)
- Smaller solutes are harder to remove with membranes
- Bench-scale systems tend to underpredict rejection



Enhanced Contact Plasma: Retentate Treatment





Batch bubble column reactor with liquid recirculation

- > Treated liquid volume: 3.1 L
- > Treatment time: 180 min
- Gas flowrate adjusted to maintain foam height
- Proprietary surfactant addition every 15 min
- Solution recirculated through heat exchanger at 10°C



Enhanced Contact Plasma: Performance Results





Concentrations of all identified precursors and long-chain PFAS were below respective detection limits (2-7 ng/L) within 20 minutes; many within 5 minutes of treatment

Enhanced Contact Plasma: Performance Results





- Short-chain PFAS removal varied from 57% to
 >99% within 150 minutes of treatment
- Sulfonates readily degrade over course of treatment while carboxylates exhibit greater treatment times
- Production of PFBA and slow decline of PFPeA can be attributed to the degradation of longchain PFAS and unidentified precursors
- For the field demo, lower flowrates and/or multiple passes will be necessary to achieve short-chain PFAS removal





- Nanofiltration achieved up to 10x concentration of source water and 88->99% PFAS separation using closed circuit desalination
- Both membranes (NF90 and CR100) operated well with little to no reductions in permeability
- Plasma achieved complete removal of identified PFAS precursors and long-chain PFAS to below detection limits; longer treatment times required for short-chain PFAS

For the field demonstration...

- Pretreatment required to manage water chemistry at the site
- Lower flowrates and/or multiple passes will be necessary to achieve short-chain PFAS removal



Next Steps: Field Demonstration





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Plasma Reactor Design & Operation

Charles Schaefer

Electrochemical Oxidation Testing

QUESTIONS?



Technical Resources



Nanofiltration

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Enhanced Contact Plasma

- Nau-Hix, C. et al. (2021). Field Demonstration of a Pilot-Scale Plasma Reactor for the Rapid Removal of Poly- and Perfluoroalkyl Substances in Groundwater. Environmental Science & Technology: Water, 1(3), 680-687.
- Singh, R. K. et al. (2019). Rapid Removal of Poly- and Perfluorinated Compounds from Investigation-Derived Waste (IDW) in a Pilot-Scale Plasma Reactor. Environmental Science & Technology, 53(19), 11375-11382.

Electrochemical Oxidation

Fang, Y. et al. (2022). Removal and destruction of perfluoroalkyl ether carboxylic acids (PFECAs) in an anion exchange resin and electrochemical oxidation treatment train. Water Research 230, 119522.



liquid. Different excitation sources including AC, nand plasma processing for water treatment applications I

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Next Steps: Destructive Technology Comparison



Objective

Direct comparison of two PFAS destructive technologies based on:

- PFAS removal efficiency
- Energy use & treatment cost (\$/gal)

"Apples to Apples" Comparison

- Both technologies will use nanofiltration concentrate generated during the field demonstration.
- Technologies will be tested under similar controlled operating conditions.
- Key elements: i) assessing PFAS defluorination relative to the applied current density (mA/cm^2) and ii) verifying the longevity of the technologies.



Enhanced Contact Plasma: Performance Results



- Concentrations of most PFAS in the CR100 permeate were below respective detection limits (Rejection = 1)
- Two exceptions: PFPeA and PFBA (Rejection = 0.96 and 0.88, respectively)

Pre-treatment:	Post-treatment:
ΣΡFAS = 55.8 μg/L	- ΣPFAS = 6.4 μg/L
TOPA = 24.2 μg/L	- TOPA = 6.3 μg/L

